

Embedded and Real-time Systems Control

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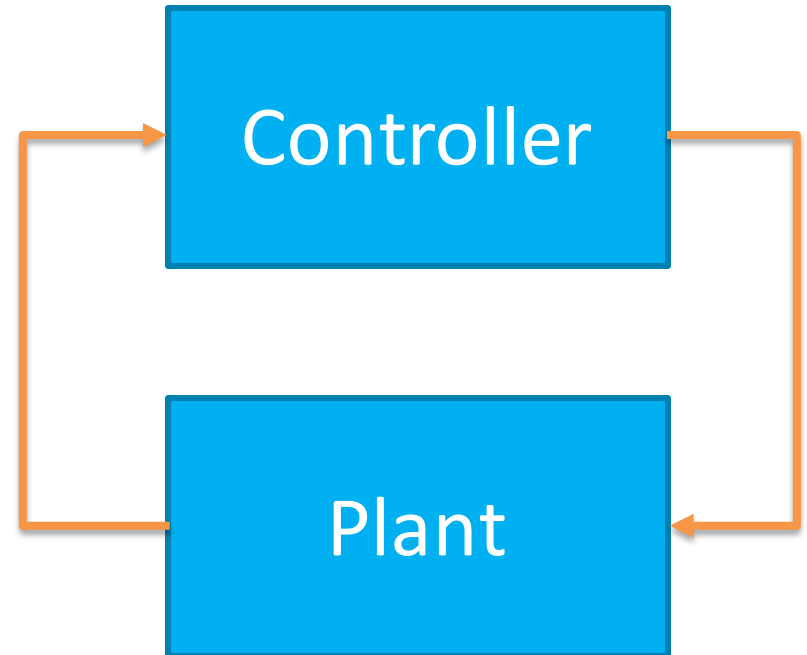


CHARLES UNIVERSITY IN PRAGUE

Faculty of Mathematics and Physics

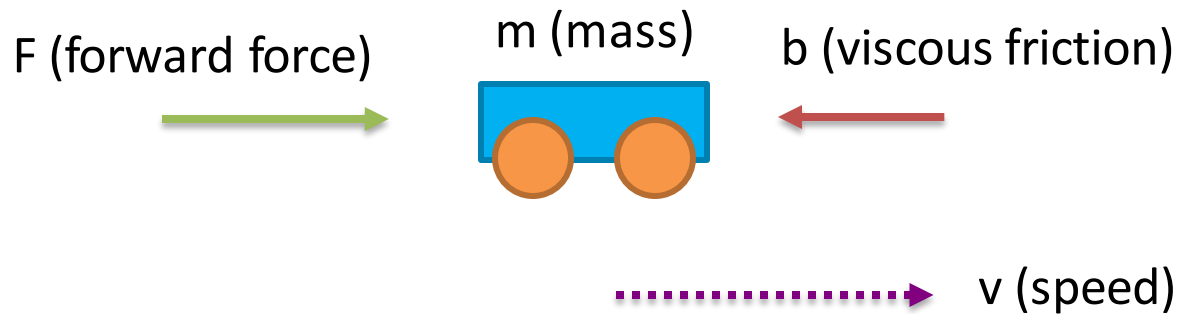
Controlling Environment

- Plant
 - continuous dynamic system
- Controller
 - discrete reactive system



- Controller brings plant to a desired state and keeps it there
- Controller keeps a setpoint (the desired state)

Example: moving body



$$\frac{\partial v}{\partial t} = \frac{F - bv}{m}$$

Task: regulate F to accelerate to a given speed and keep the speed

Modeling using block diagram

- Block is a function
 - Input/output ports
 - Some blocks may have internal state (e.g. integrator)
- Connections
 - Data flow between ports
- Simulink (an extension to MATLAB) to model a system using blocks
 - Simulation, analysis, code generation
- Example: `moving_body_1_no_controller.slx`

Simple relay control

- Switch maximum force on/off
 - Example: moving_body_2_relay.slx
- Fails when there is a lag in the system
 - e.g. because of delayed actuation or because of periodic sampling/actuation
 - Example: moving_body_3_lag_relay.slx

PID Controller

- Typical controller for linear state space systems
 - Linear state-space systems is a system that can be described by the following differential equation:

$$\frac{dx}{dt} = Ax + Bu, \quad y = Cx + Du$$

- Example (moving body): $\frac{\partial v}{\partial t} = \frac{F - bv}{m}$

$$\frac{dx}{dt} = -\frac{b}{m}x + \frac{1}{m}F, \quad v = 1x + 0F$$

PID Controller

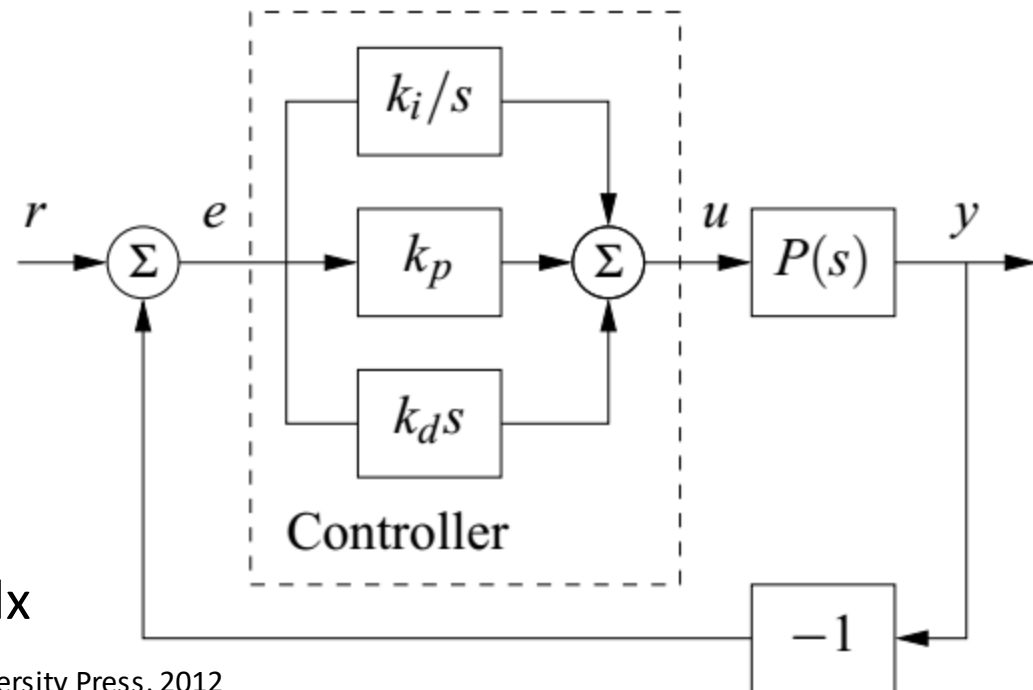
- Ideal form:

$$u = k_p e + k_i \int_0^t e(\tau) d\tau + k_d \frac{de}{dt}$$

- Weighted sum of three terms:

- Proportional
- Integral
- Differential

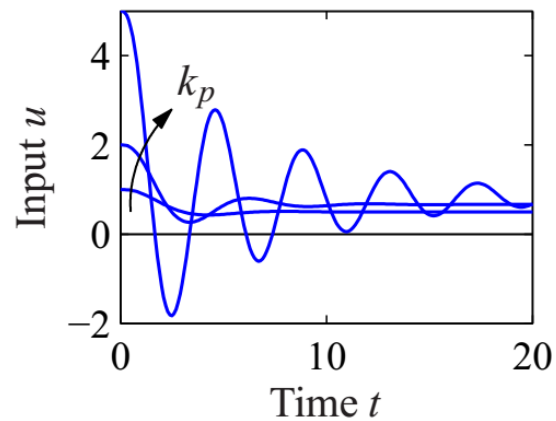
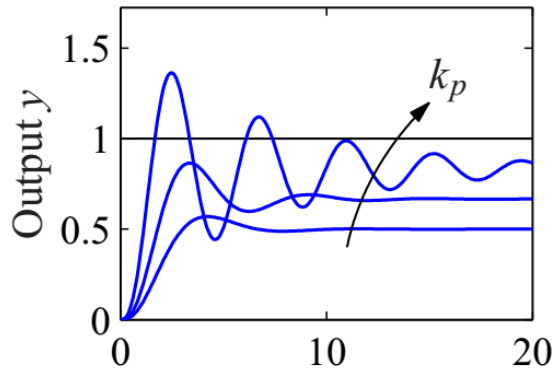
- Example: moving_body_4_pi.slx



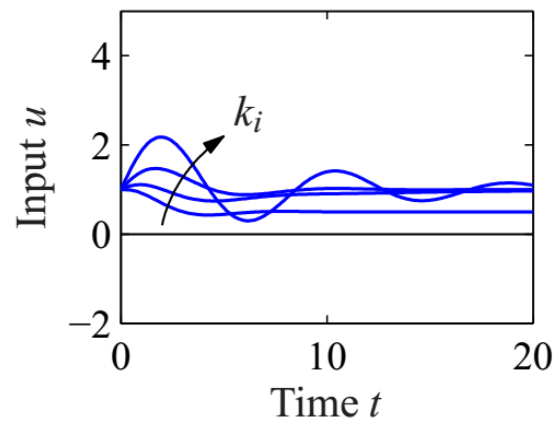
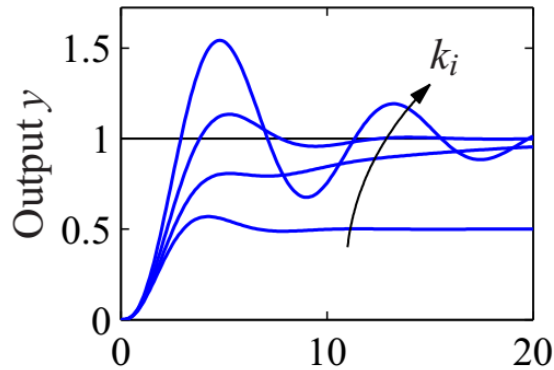
Proportional term

- Counter-acts proportionally to the error
- Low k_p
 - Slow action
- High k_p
 - May overshoot and oscillate
- Problem
 - Never reaches the set-point if there is a steady resistance
 - Can be mitigated by an extra feedforward term, but this term may vary with the internal state of the system
 - e.g. the viscous friction
- Example: `vehicle_speed_1_p.slx`

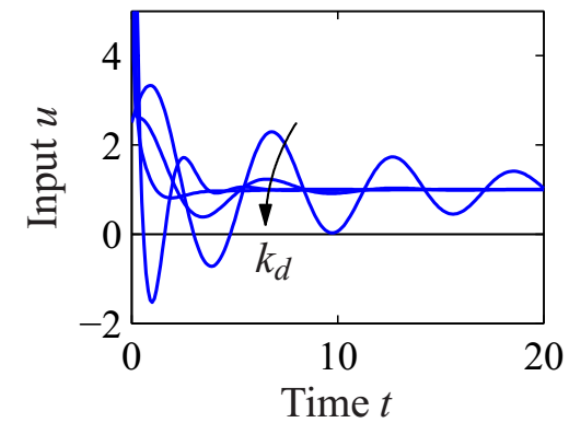
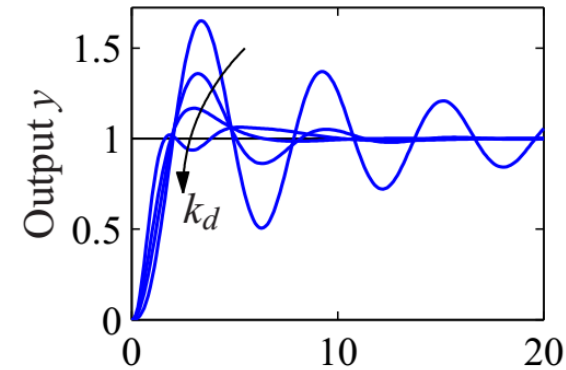
Effect of constants in PID



(a) Proportional control



(b) PI control

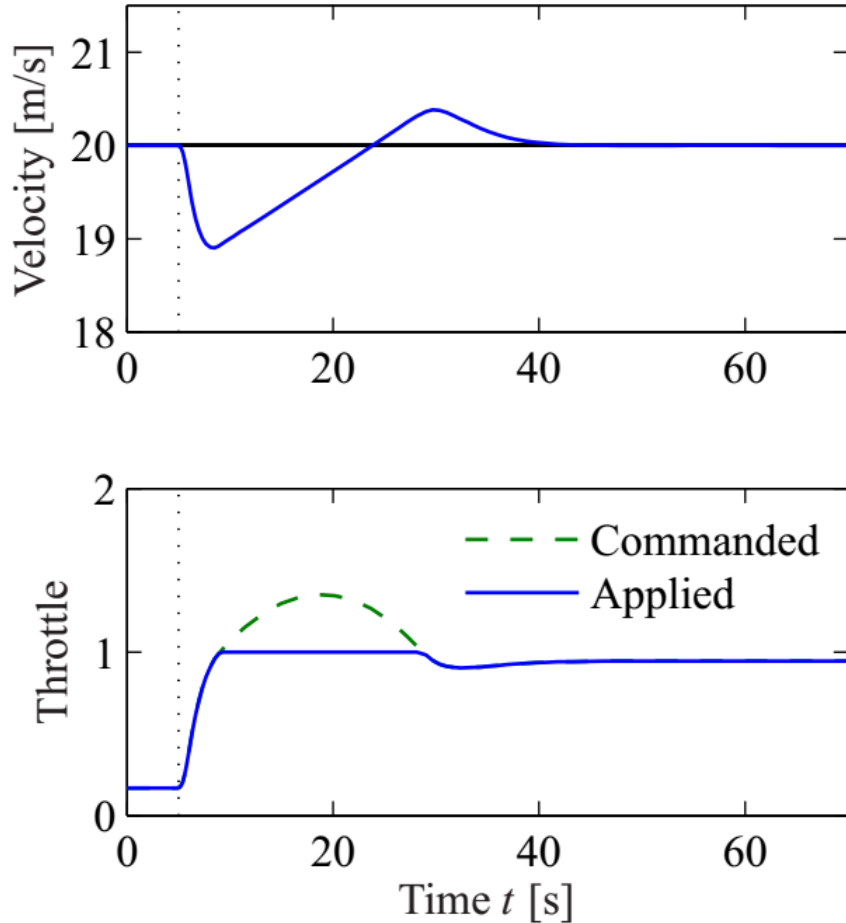


(c) PID control

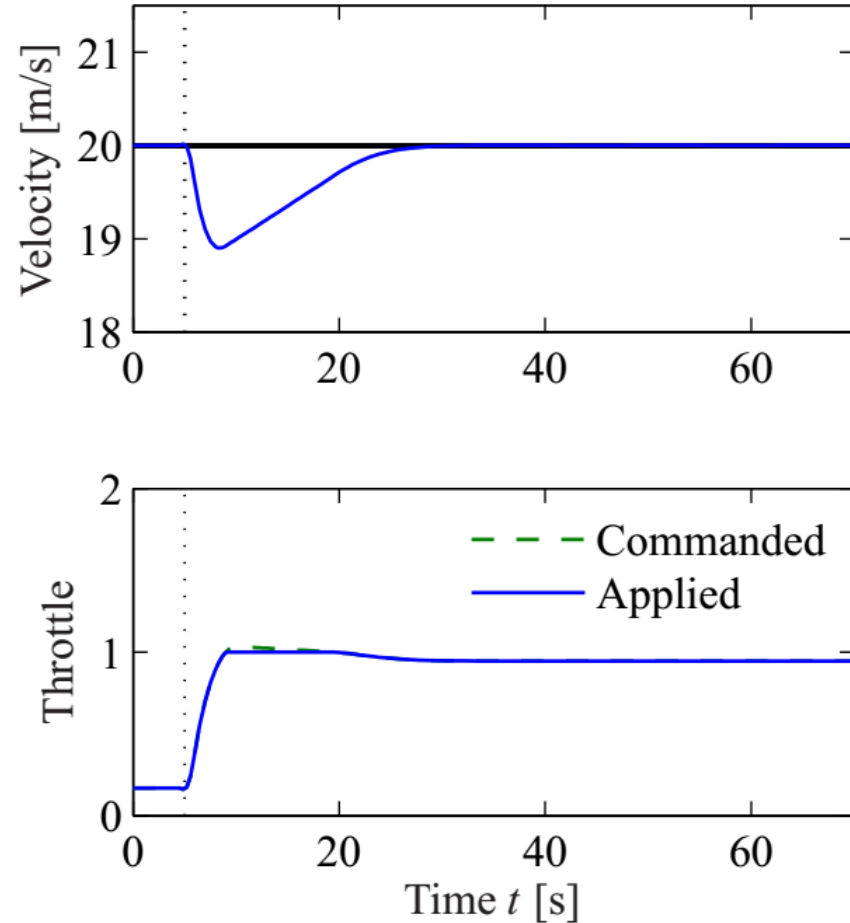
Integral term

- Mitigates the steady-state error
- Low k_i
 - Slow gradual “learning”
- High k_i
 - Big overshoot and oscillation
- Example: `vehicle_speed_2_pi.slx`
 - Note that pure I controller would work too, just slower
- Problem – integrator windup
 - Happens when actuator reaches the saturation limit
 - Integrator mistakenly accumulates value
 - Example: `vehicle_speed_3_pi_windup.slx`

Integrator windup



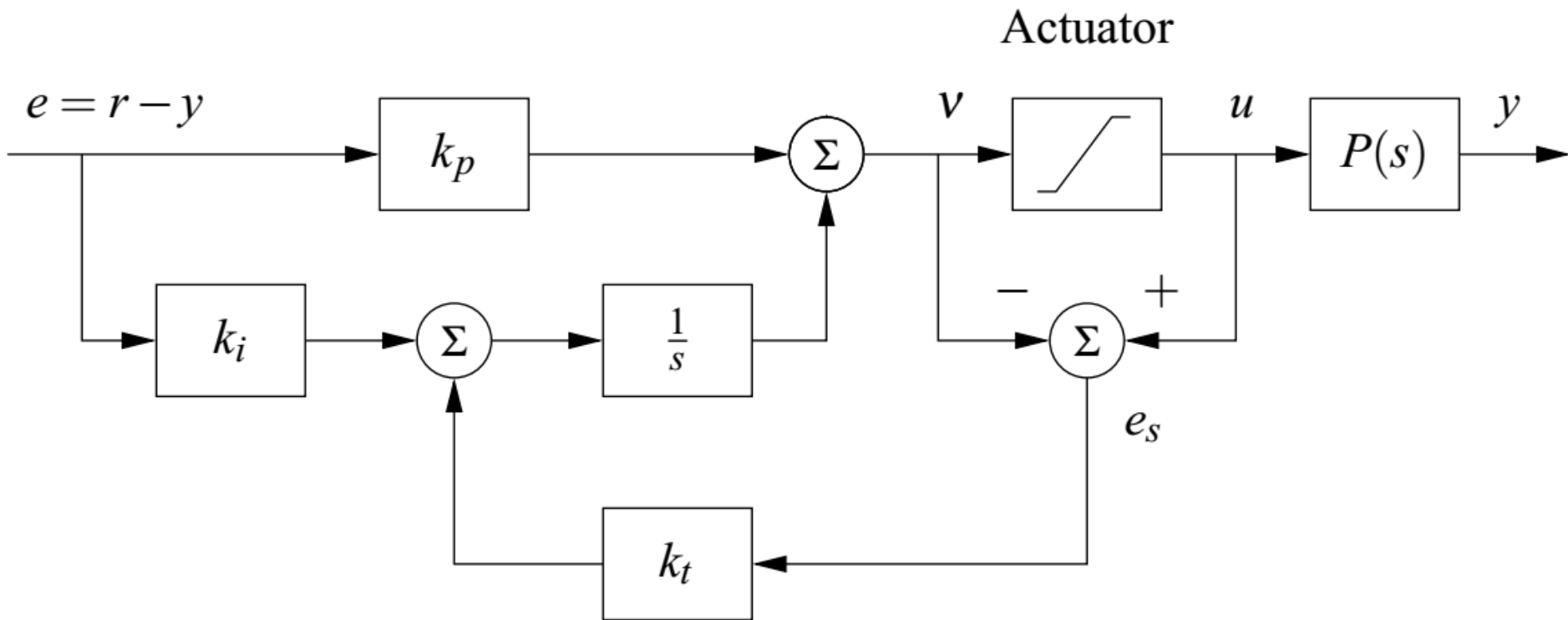
(a) Windup



(b) Anti-windup

Anti-windup

- Prevents the integrator to accumulate when saturation is reached
- Example: vehicle_speed_4_pi_anti_windup.slx



Transfer functions

- Differential and integral blocks described using transfer function $G(s)$
- $G(s) = \frac{u}{y}$
 - u ... output from the controller / input to the plant
 - y ... output from the plant
- Transfer function describes the effect on frequency and phase of a periodic signal
 - $|G(i\omega)|$... gain
 - $\angle G(i\omega)$... phase shift

Transfer functions – Bode plot

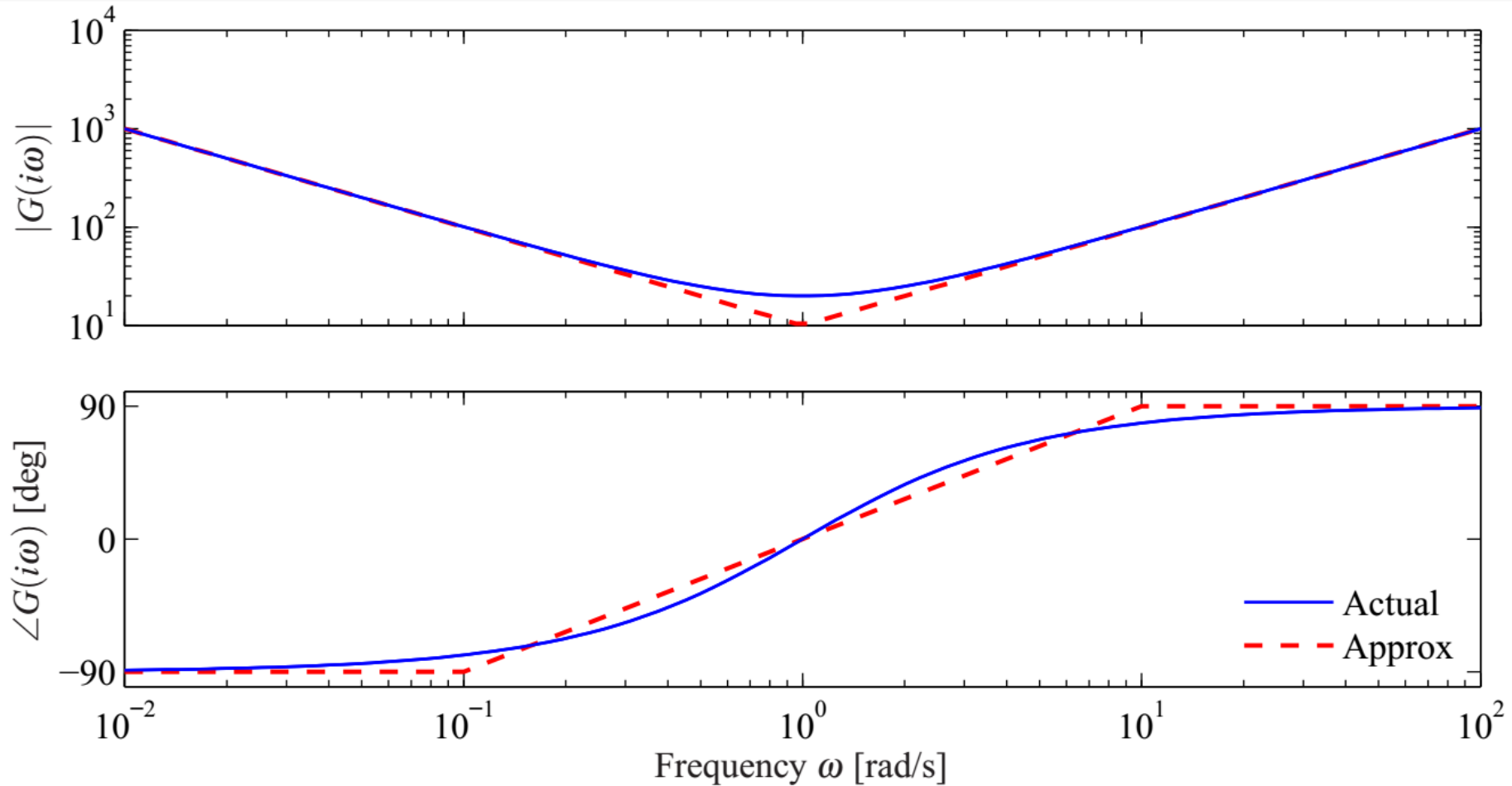


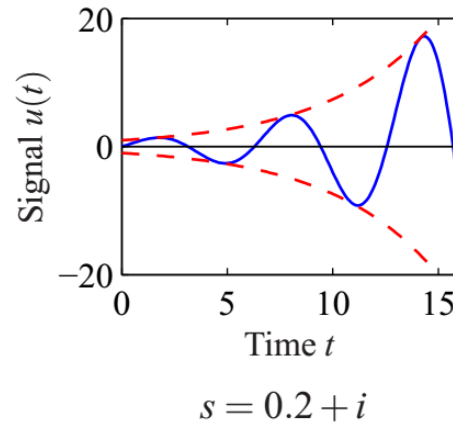
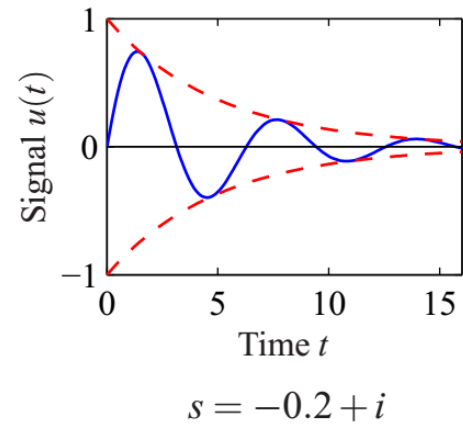
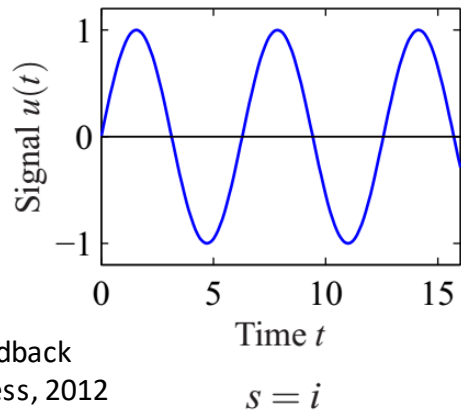
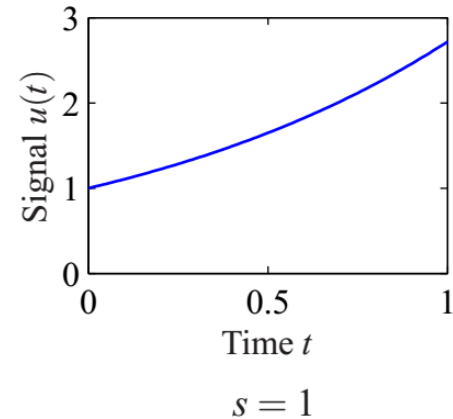
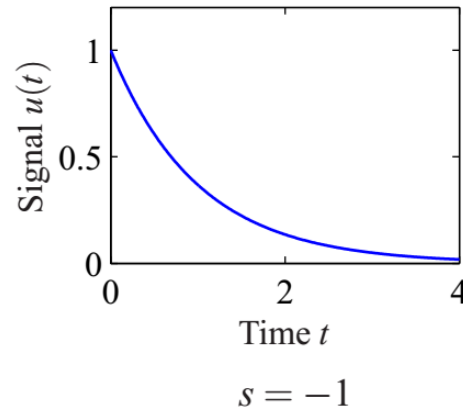
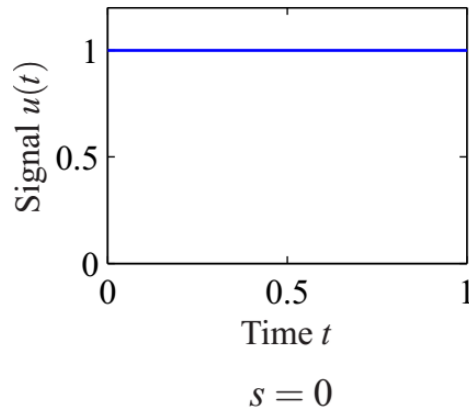
Figure 8.11: Bode plot of the transfer function $C(s) = 20 + 10/s + 10s$ corresponding to an ideal PID controller. The top plot is the gain curve and the bottom plot is the phase curve.

Transfer functions – examples

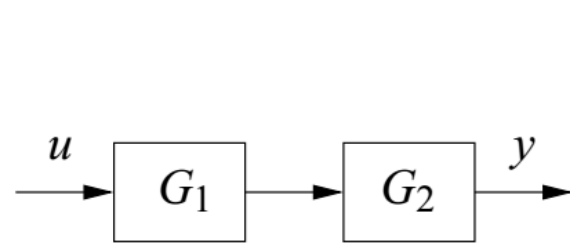
Type	ODE	Transfer Function
Integrator	$\dot{y} = u$	$\frac{1}{s}$
Differentiator	$y = \dot{u}$	s
First-order system	$\dot{y} + ay = u$	$\frac{1}{s + a}$
Double integrator	$\ddot{y} = u$	$\frac{1}{s^2}$
Damped oscillator	$\ddot{y} + 2\zeta\omega_0\dot{y} + \omega_0^2y = u$	$\frac{1}{s^2 + 2\zeta\omega_0s + \omega_0^2}$
PID controller	$y = k_p u + k_d \dot{u} + k_i \int u$	$k_p + k_d s + \frac{k_i}{s}$
Time delay	$y(t) = u(t - \tau)$	$e^{-\tau s}$

Variable s

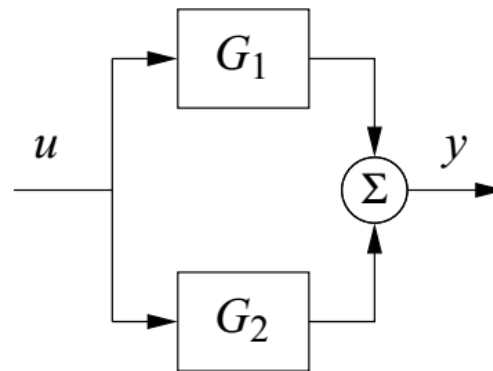
- Exponential (periodic) signal e^{st}
 - $s = \sigma + i\omega$ is a complex variable
 - σ ... decay rate (if $\sigma < 0$), ω ... frequency



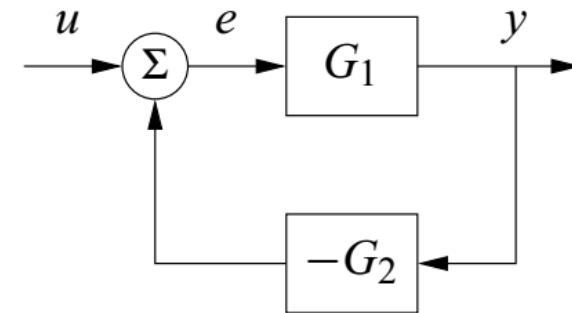
Transfer functions – block diagrams



(a) $G_{yu} = G_2 G_1$



(b) $G_{yu} = G_1 + G_2$



(c) $G_{yu} = \frac{G_1}{1 + G_1 G_2}$

Figure from Åström, Murray: Feedback Systems, Princeton University Press, 2012

Proof of
case (c):

$$\begin{aligned} y &= G_1 e, \quad e = u - G_2 y \\ y &= G_1 u - G_1 G_2 y \\ y(1 + G_1 G_2) &= G_1 u \end{aligned}$$

$$y = \frac{G_1}{1 + G_1 G_2} u$$

Derivative term

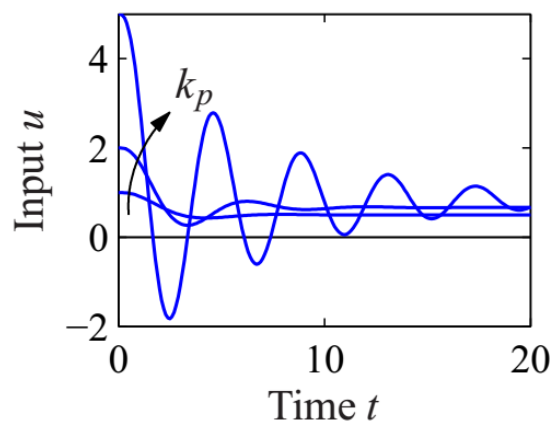
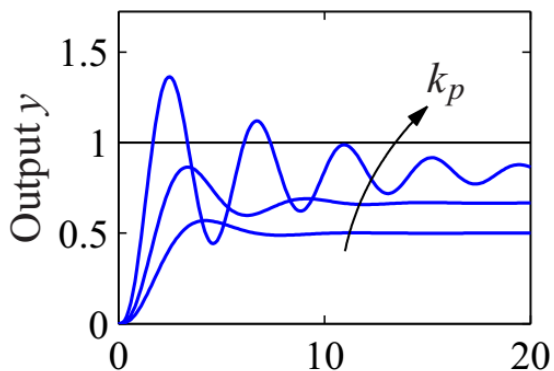
- Provides prediction of error in the future
 - Does linear extrapolation
- Reduces oscillations and overshoot

- Low k_d
 - Small effect on oscillations
- High k_d
 - Reduces controller response
 - May itself create oscillations

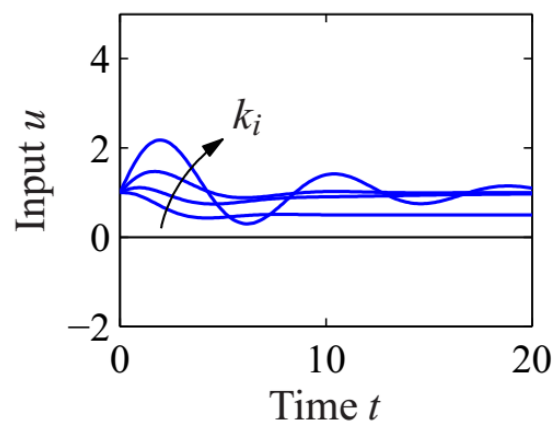
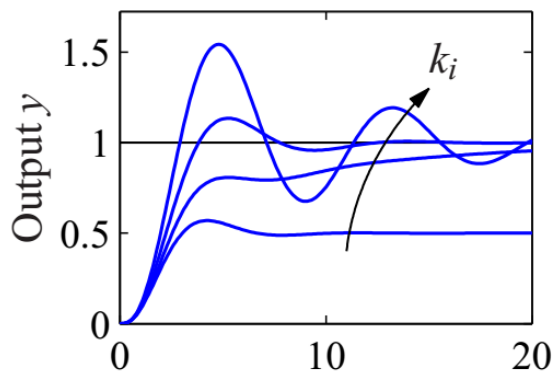
- Examples: vehicle_position_1_p.slx, vehicle_position_2_pd.slx, vehicle_position_3_pid.slx

- Problem – sensitivity to high frequencies (noise)
 - Derivative term amplifies the high frequencies
 - Mitigated by low-pass filtering

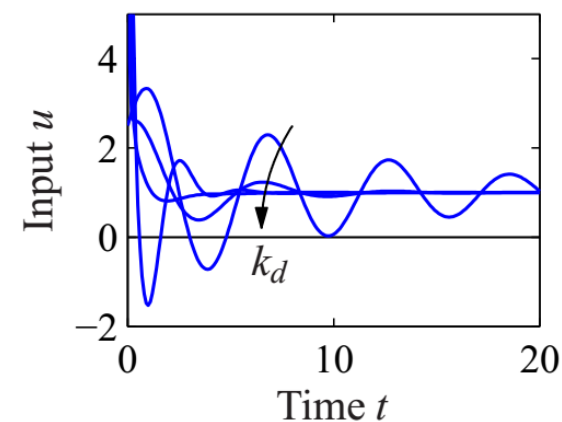
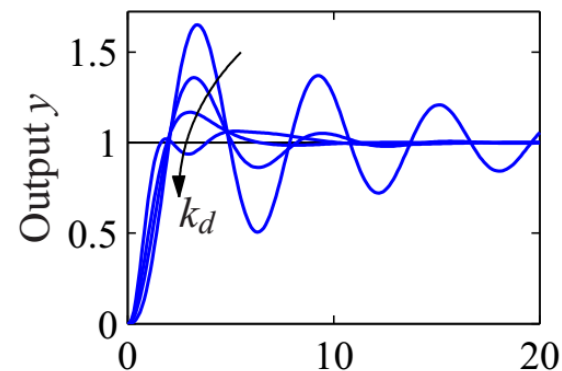
Effect of constants in PID



(a) Proportional control



(b) PI control

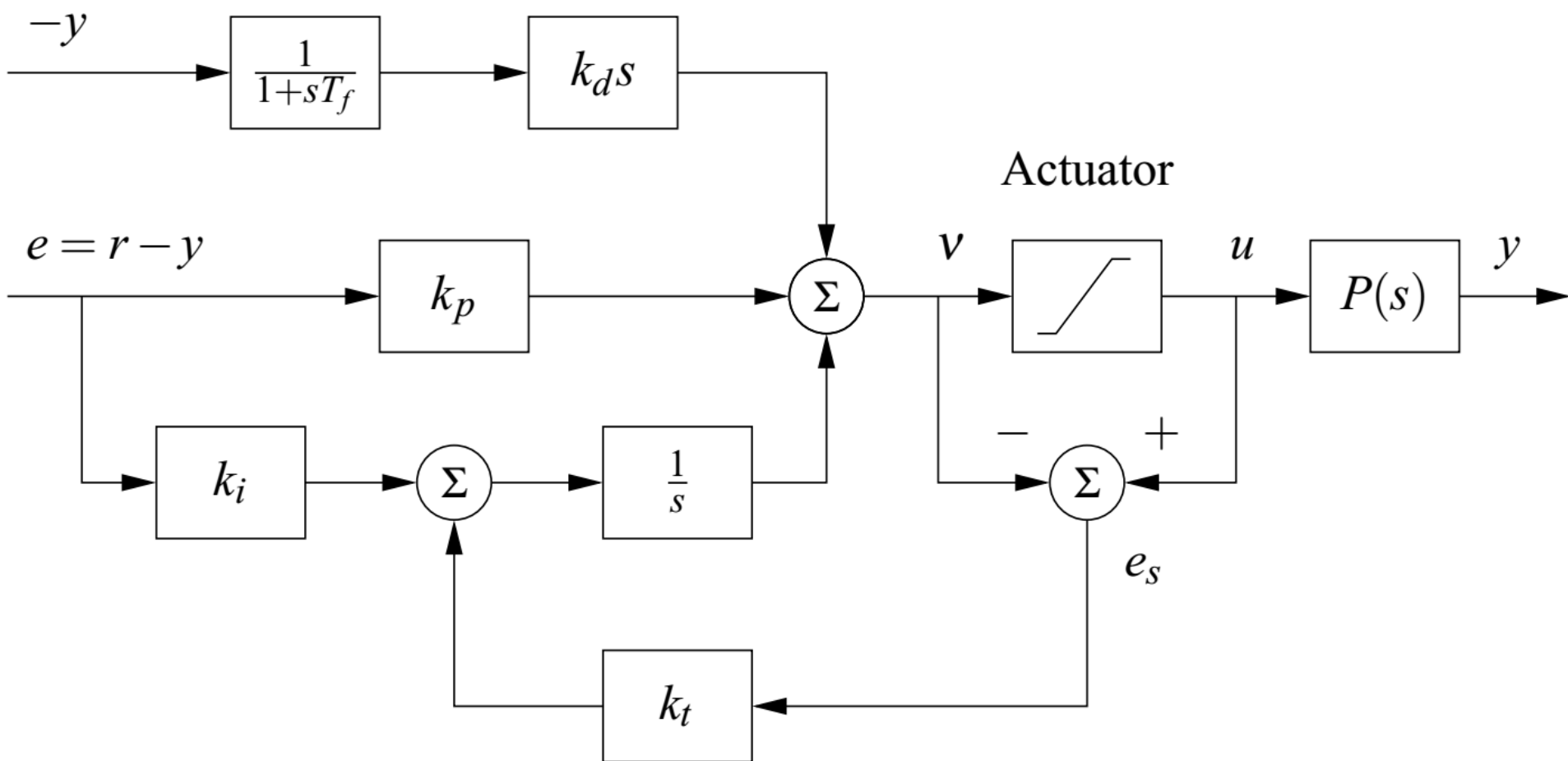


(c) PID control

Filtered derivative

- Derivative term $D = k_d s$ replaced by $D = k_d \frac{s}{1+T_f s}$
 - for small frequencies acts as derivative
 - for high frequencies acts as a constant gain
- To mitigate spike when setpoint r is changed, it can take $-y$ as the input (instead of $e = r - y$)
 - For constant setpoint, the computation is the same because r as a constant gets discarded in the differential

Filtered derivative

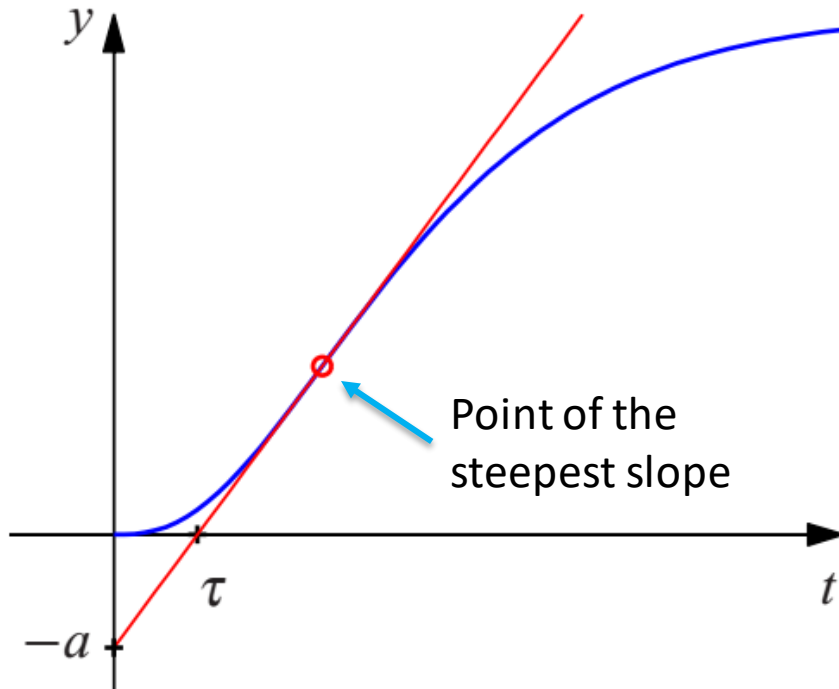


Tuning

- Different methods for initial estimation of the constants k_p, k_i, k_d
- Manual fine-tuning may be required

Ziegler-Nichols step response method

Unit step is applied
and response measured



Constants for controller

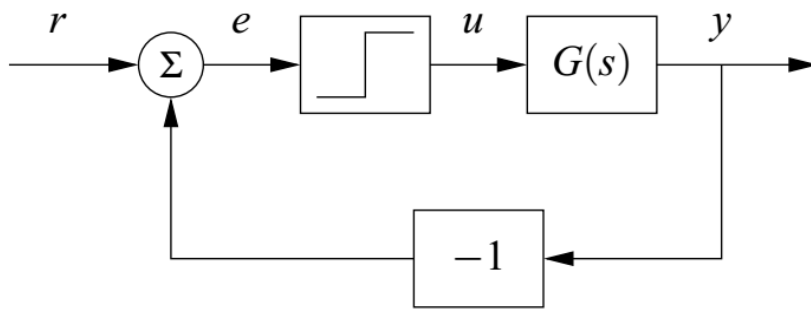
$$u = k_p \left(e + \frac{1}{T_i \int_0^t e(\tau) d\tau} + T_d \frac{de}{dt} \right)$$

computed as:

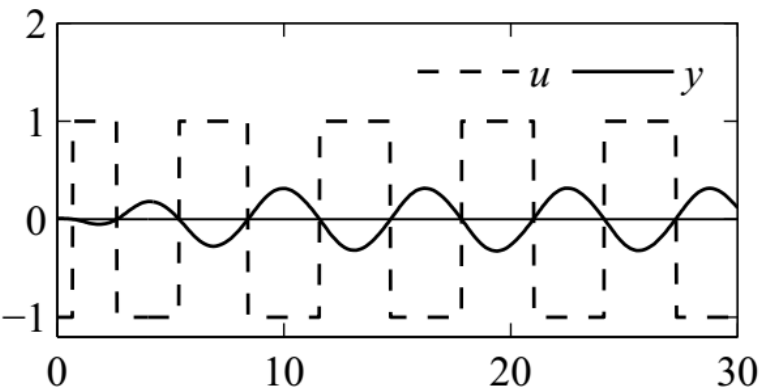
Type	k_p	T_i	T_d
P	$1/a$		
PI	$0.9/a$	3τ	
PID	$1.2/a$	2τ	0.5τ

Ziegler-Nichols frequency response

Using relay feedback to bring the system to oscillation



Oscillatory response



Constants for controller

$$u = k_p \left(e + \frac{1}{T_i} \int_0^t e(\tau) d\tau + T_d \frac{de}{dt} \right)$$

computed as:

Type	k_p	T_i	T_d
P	$0.5k_c$		
PI	$0.4k_c$	$0.8T_c$	
PID	$0.6k_c$	$0.5T_c$	$0.125T_c$

where:

T_c ... oscillation period

d ... relay amplitude

a ... process amplitude

$K_c = \frac{4d}{a\pi}$... critical gain

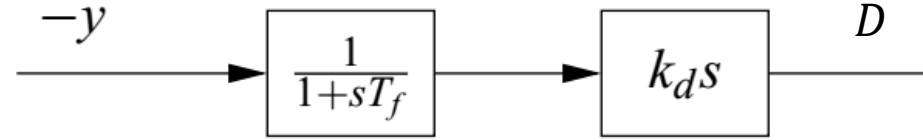
Implementation

- $P(t_k) = k_p (r(t_k) - y(t_k))$
- $I(t_{k+1}) = I(t_k) + k_i h e(t_k) + k_t h (\text{sat}(v) - v)$
 - h is the discrete time step
- $D(t_k) = \frac{T_f}{T_f + h} D(t_{k-1}) - \frac{k_d}{T_f + h} (y(t_k) - y(t_{k-1}))$
 - steps to arrive at D on the next slide

Steps to derive $D(t_k)$

$$D = -\frac{y k_d s}{1 + s T_f}$$

$$D + T_f D s = -k_d y s$$



Applying the transfer function s on the respective terms:

$$T_f \frac{dD}{dt} + D = -k_d \dot{y}$$

Approximating the derivative with backward difference

$$T_f \frac{D(t_k) - D(t_{k-1})}{h} + D(t_k) = -k_d \frac{y(t_k) - y(t_{k-1})}{h}$$

Pseudo-code

```
% Precompute controller coefficients
```

```
bi = ki * h
```

```
ad = Tf / (Tf + h)
```

```
bd = kd / (Tf + h)
```

```
br = kt * h
```

```
% Control algorithm - main loop
```

```
while (running) {
```

```
  r = adin(ch1)
```

```
  y = adin(ch2)
```

```
  P = kp * (r - y)
```

```
  D = ad * D - bd * (y - yold)
```

```
  v = P + I + D
```

```
  u = sat(v, ulow, uhigh)
```

```
  daout(ch1)
```

```
% read setpoint from ch1
```

```
% read process variable from ch2
```

```
% compute proportional part
```

```
% update derivative part
```

```
% compute temporary output
```

```
% simulate actuator saturation
```

```
% set analog output ch1
```

```
  I = I + bi * (r - y) + br * (u - v)
```

```
  yold = y
```

```
% update integral
```

```
% update old process output
```

```
  wait_for_next_period
```

```
}
```

Removing non-linearities

- Sometimes the process has non-linearities
 - E.g. coulomb friction (can be modeled as a relay)
- Can be addressed by conditioning the process
 - E.g. adding compensation to the coulomb friction to output of the controller